

Supporting Information for

# **Fibrous MXene Aerogels with Tunable Pore Structures for High-Efficiency Desalination of Contaminated Seawater**

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## **S1 Supplementary Methods**

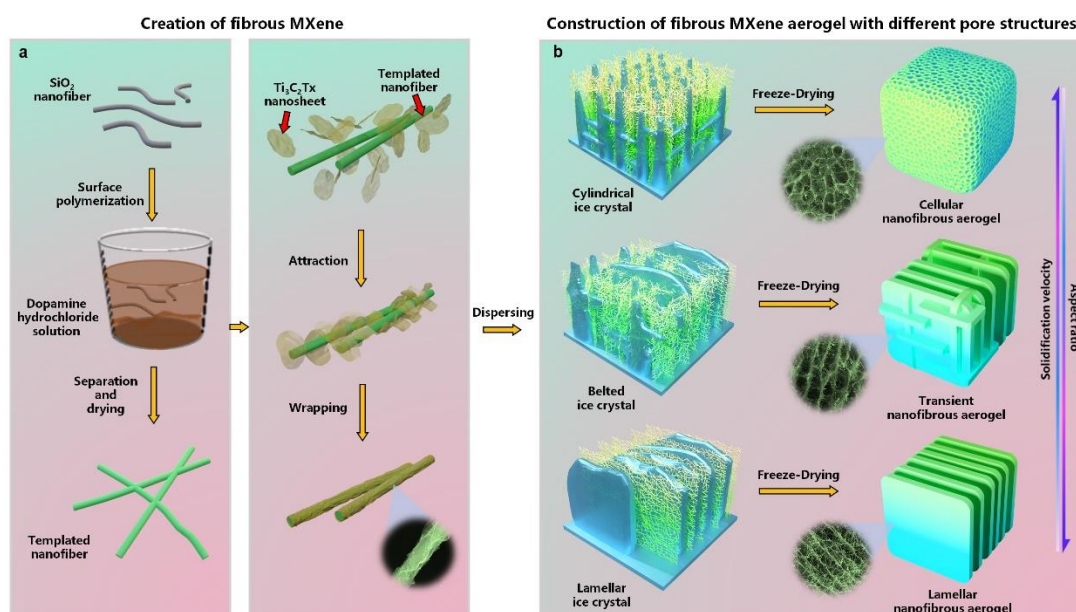
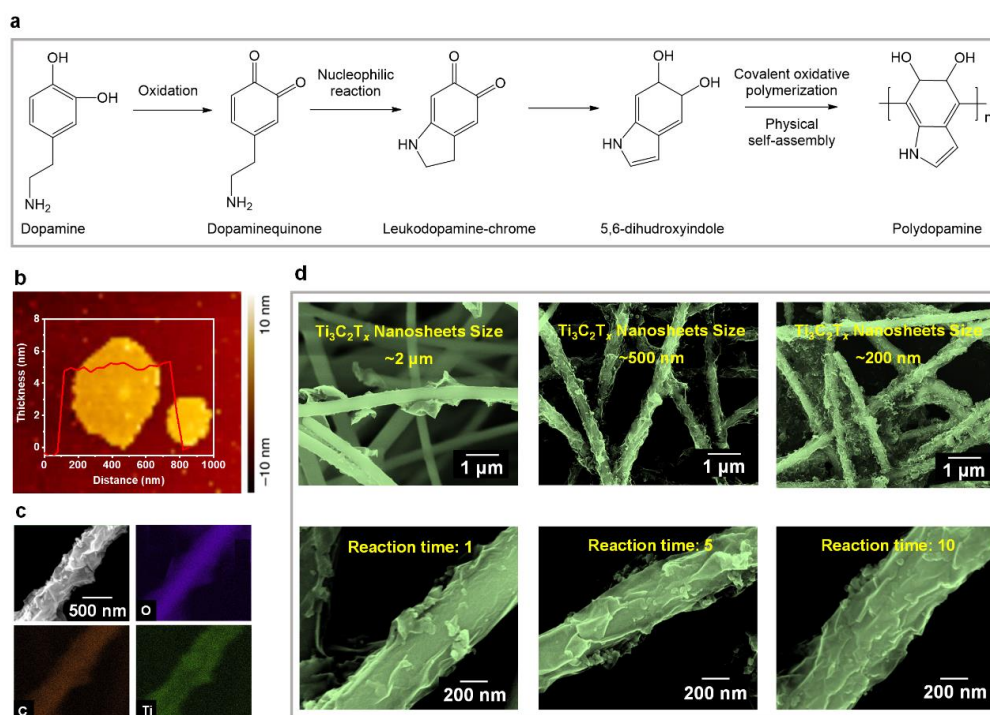
### **S1.1 Simulated Seawater Preparation**

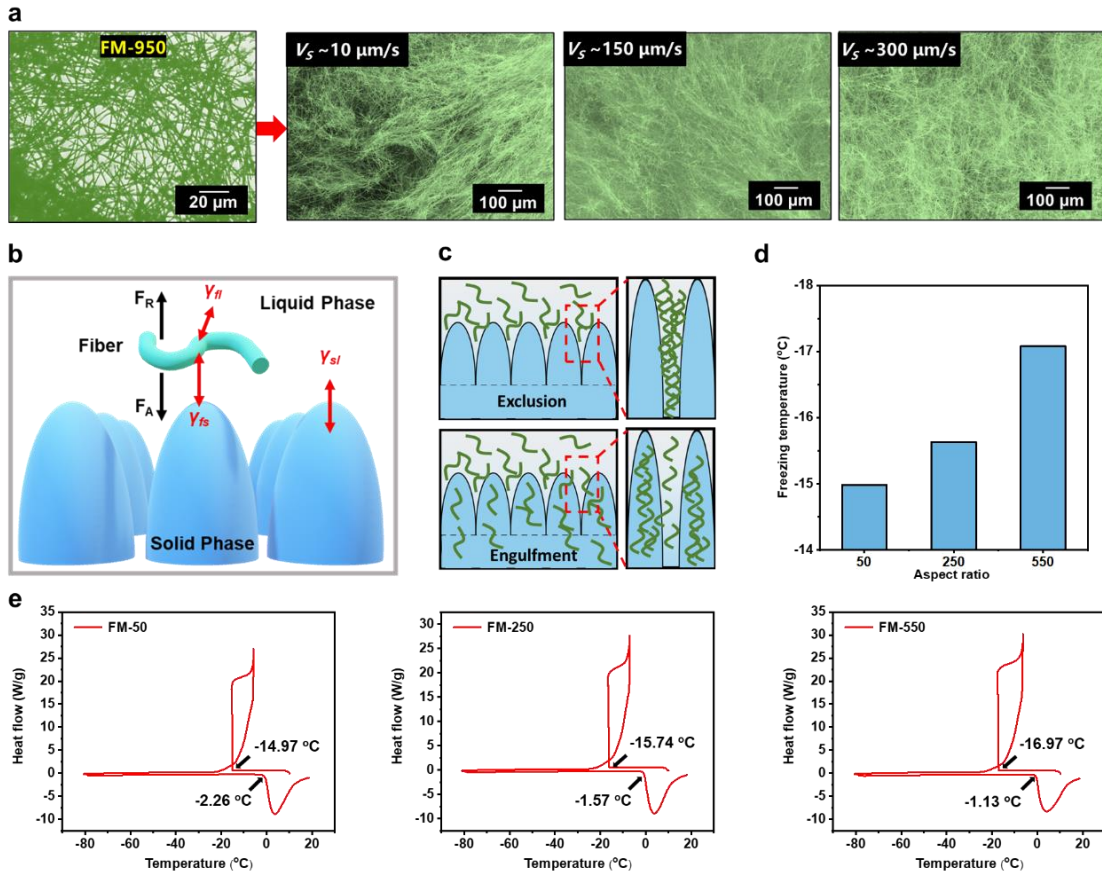
26.5 g of sodium chloride (NaCl), 24 g of magnesium chloride (MgCl<sub>2</sub>), 0.73 g of potassium chloride (KCl), 3.3 g of magnesium sulfate (MgSO<sub>4</sub>), 0.2 g of sodium bicarbonate (NaHCO<sub>3</sub>), 1.1 g of calcium chloride (CaCl<sub>2</sub>), and 0.28 g of sodium bromide (NaBr) were mixed with 1 L of deionized water to obtain simulated seawater with a pH of 7.02.

### **S1.2 Characterizations**

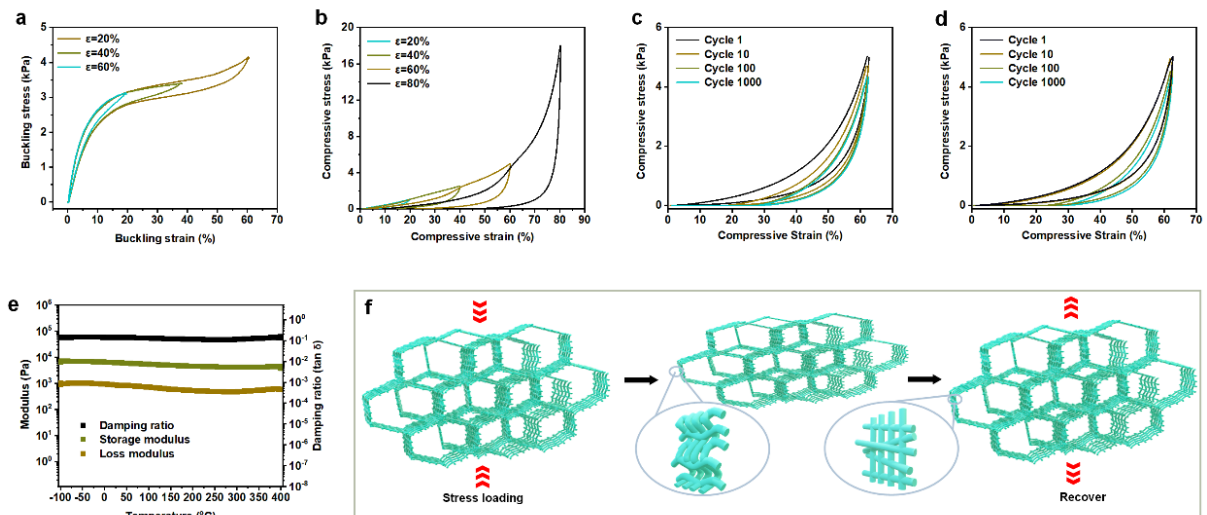
SEM was carried out by a Hitachi S-4800 microscope. TEM was carried out by a JEOL JEM-2100F microscope. AFM was carried out by a Bruker MM8 microscope. Optical photos were recorded by an Olympus BH2-UMA microscope. XRD was carried out by an Advance D8 diffractometer with Cu K $\alpha$  radiation ( $\lambda = 1.5406 \text{ \AA}$ ). XPS was carried out by a ULVAC-PHI Quantera SXM spectrometer. Raman was carried out by a Renishaw spectrometer ( $\lambda = 633 \text{ nm}$ ). UV-vis-NIR was carried out by a Shimadzu UV-3600 spectrophotometer. The compression–recovery and buckling–recovery tests were performed by a DMA (Q850, TA Instruments). The in-situ bending test was performed by an FIB-SEM (Crossbeam340, Carl Zeiss). The underwater oil contact angle was recorded by a contact angle goniometer (SL 200B, Kino). The thermal conductivity was recorded by a Hot Disk instrument (TPS2500S, Hot disk). The infrared images were captured by an infrared camera (TiS75, Fluke). The crystallization temperature was measured by a DSC (200 F3, Netzsch). The concentrations of salt ions were measured by ICP-AES (Leeman Prodigy).

## S2 Supplementary Figures

Scheme S1 **a** Creation of 1D FMs. **b** Construction of FMAs with tunable pore structures**Fig. S1** **a** Polymerization reaction of dopamine. **b** AFM images of  $\text{Ti}_3\text{C}_2\text{T}_x$  nanosheets. **c** EDS maps of an individual FM. **d** SEM images of FMs with different sizes of  $\text{Ti}_3\text{C}_2\text{T}_x$  nanosheets and reaction times

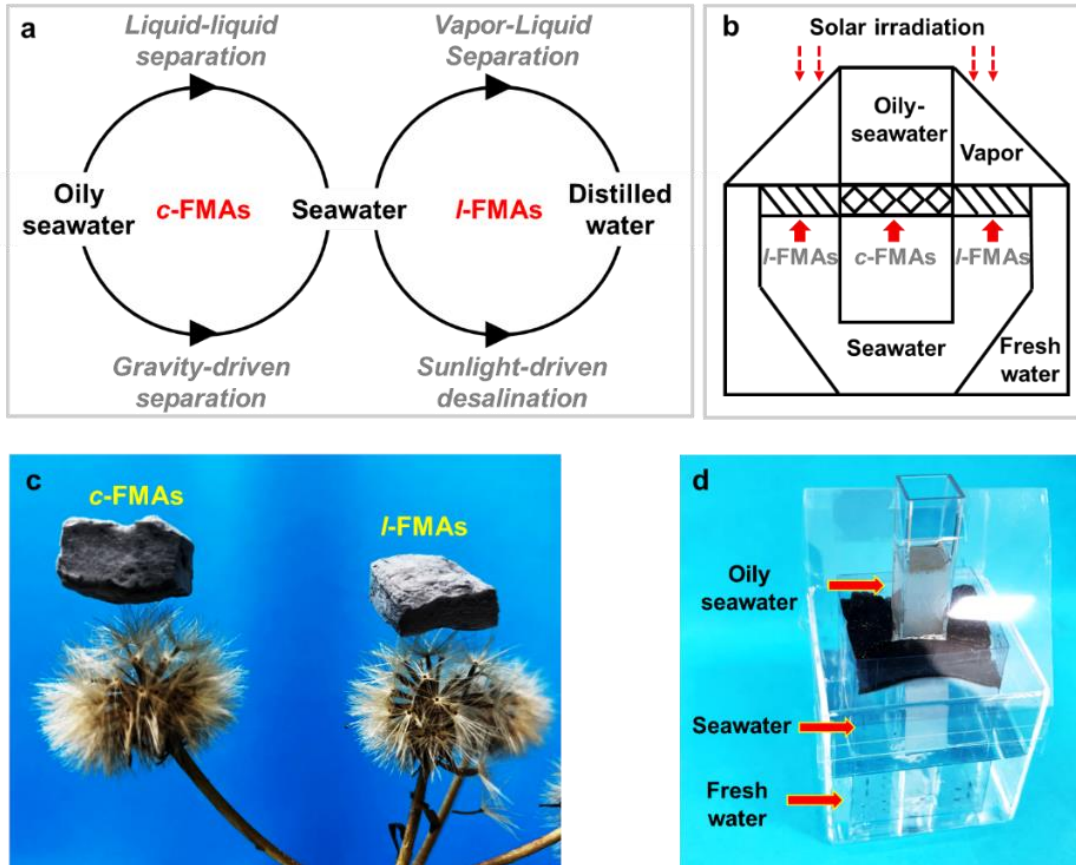


**Fig. S2** **a** Pore structures of FMAs constructed from FM-950 by regulation of solidification velocity. **b** Schematic illustration of forces acting on an individual FM in the vicinity of a freezing front. **c** Schematic illustration of exclusion or engulfment state of FMs. **d** Comparison of freezing temperatures of FMs with different aspect ratios. **e** DSC thermograms of FM-50, FM-250, and FM-550 dispersions during the cooling process

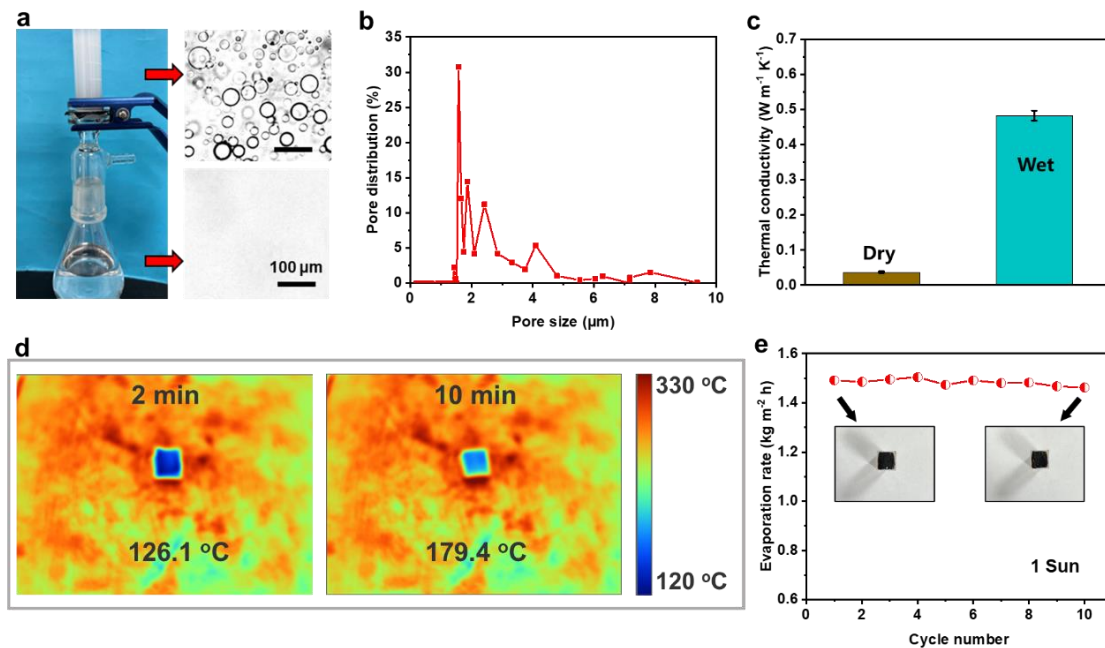


**Fig. S3** **a** Buckling stress–strain curves of *l*-FMAs with increasing strain (0 to 60%). **b** Compressive stress–strain curves of *l*-FMAs with increasing strain (0 to 80%). **c** 1000-cycle fatigue test with 60% compressive strain of *l*-FMAs. **d** 1000-cycle fatigue test with 60% compressive strain of *c*-FMAs. **e** Temperature dependence of storage modulus, loss modulus, and damping ratio for *c*-FMAs. **f** Schematic models showing the compression–recovery behavior of cellular pore structure

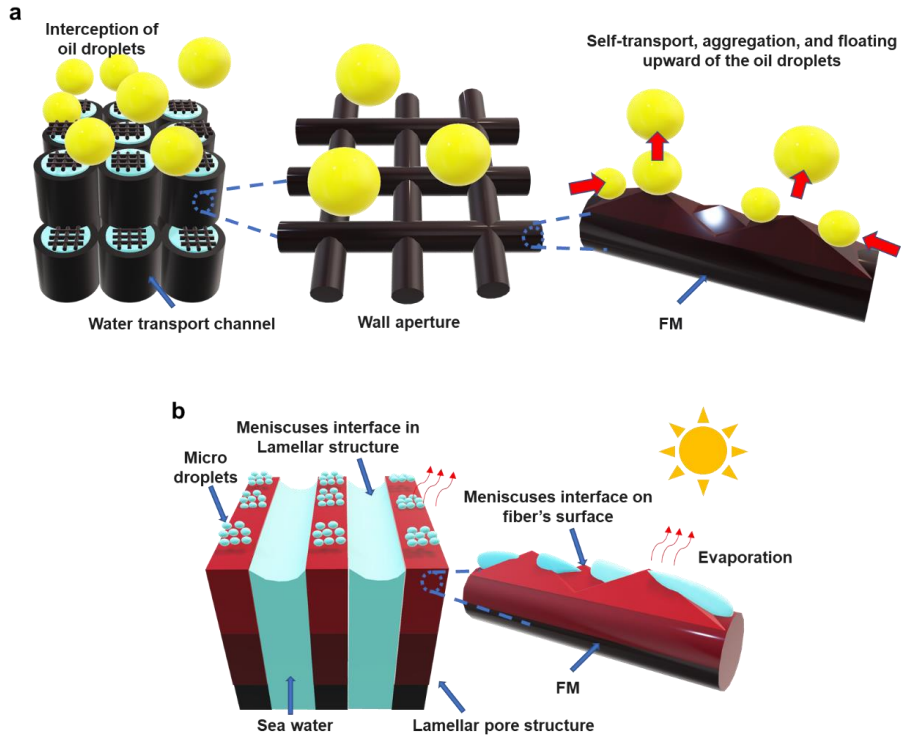




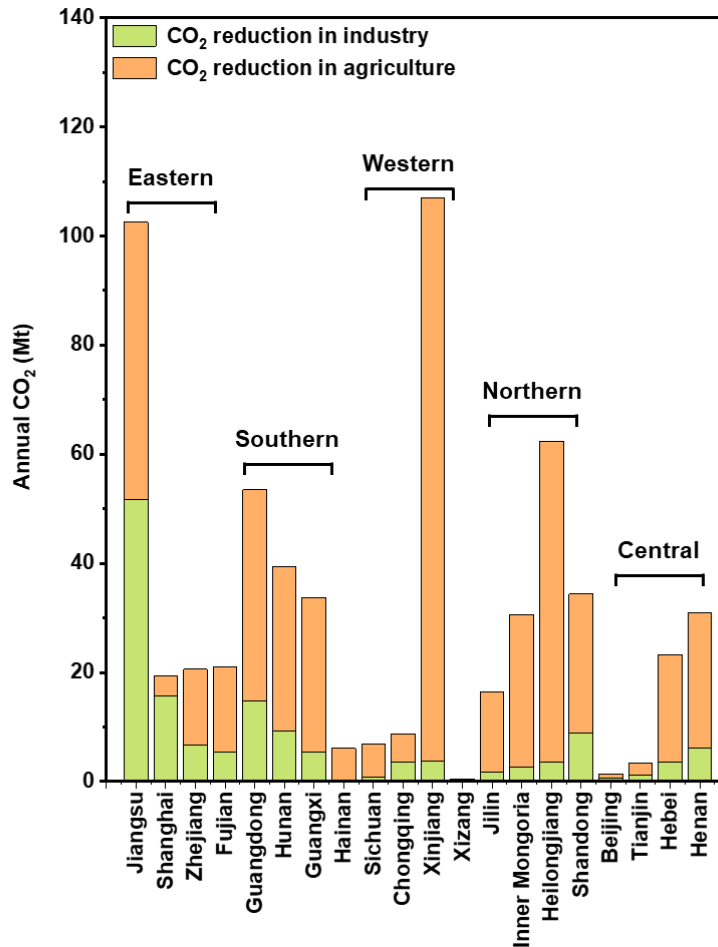
**Fig. S4** **a** and **b** Concept diagram of dual-cycle desalination system. **c** Optical photo of *c*-FMAs and *l*-FMAs. **d** Demo of modularized solar evaporator



**Fig. S5** **a** Separation apparatus by gravity-driven separation of oil-in-water emulsions using *c*-FMAs, and the corresponding microscopic images of emulsions before and after separation. **b** Pore size distribution of *c*-FMAs. **c** Thermal conductivity of *l*-FMAs in the dry and wet states. **d** Infrared images of *l*-FMAs placed on a hot desk for 10 min. **e** Stability of *l*-FMAs under one sun over 10 cycles (1 h for each cycle). The inset in **e** shows the surface states of *l*-FMAs in the 1<sup>st</sup> and 10<sup>th</sup> cycles



**Fig. S6** **a** Multi-sieving effect in *c*-FMAs. **b** Multi-meniscuses evaporation interfaces in *l*-FMAs



**Fig. S7** Annually averaged CO<sub>2</sub> reduction in industry and agriculture over different regions in China as simulated based on our modularized solar evaporator

## S3 Supplementary Tables

Table 1

Average aspect ratio	Rotational speed (Shearing, r/min)	Shearing time (min)	Number of cycles	Rotational speed (Centrifugation, r/min)	Centrifugation time (min)
50	10000	1	20	6000	8
250	7000	1	10	4500	8
550	7000	1	6	4500	8
950	3000	1	2	/	/

Table 2

Province	Productivity of thermal power generation (kWh)	Productivity of hydroelectric power generation (kWh)	Productivity of wind power generation (kWh)	Productivity of nuclear power generation (kWh)	Productivity of solar power generation (kWh)	Industrial water consumption (Billion m <sup>3</sup> )	Agricultural water consumption (Billion m <sup>3</sup> )
Beijing	444.6	12.8	0.1	0	1.5	2.9	2.8
Tianjin	497.7	0	10	0	6.01	4.8	9.3
Shanghai	454.5	0	8.4	0	0.31	65	15.3
Chongqing	344.1	112.4	8.2	0	2.14	19.3	28.7
Hebei	2222.5	5.9	354.1	0	105.7	17.7	97.1
Henan	1231.7	44.4	95.4	0	25.49	28	115
Yunnan	343.8	2218.6	173.9	0	27.39	15.7	112.1
Liaoning	1350.1	33.9	171.4	358.5	25.7	16.5	77.2
Heilongjiang	850.3	25.2	118.8	0	33.2	17.8	289.2
Hunan	904.4	460.7	125.2	0	15.7	62.1	199.9
Anhui	2690.3	55.7	85.6	0	80.3	82.1	144.1
Shandong	3464	6.3	204.1	134.6	49.59	40.3	115.8
Xinjiang	3014.2	217.5	427.1	0	127.7	18.7	527.9
Jiangsu	4004	26.3	288.8	400.2	68.1	250.2	246.2
Zhejiang	2770.8	146.4	36.5	664.6	47.5	35.8	73.3
Jiangxi	1117.5	60	77	0	38	48.7	167.3
Hubei	978.7	966.7	66.6	0	30.22	85.6	177.7
Guangxi	597.8	251.1	61.8	93.1	5.98	36.5	189.6
Gansu	678.3	213.8	187.5	0	75.58	6.5	82.6
Shanxi	2378.2	25.5	254.5	0	89.46	12.3	40.8
Inner Mongolia	3639.3	36.2	617.2	0	106.19	13.4	137.5
Shaanxi	2041.4	110.7	126.4	0	74.6	10.9	54.6
Jilin	483.5	62	80.2	0	19.98	9.2	79.9
Fujian	1711	181.1	134.9	777.2	4	35.4	99.8
Guizhou	748	335.5	45.6	0	27.03	20	62.1
Guangdong	2220.2	64.6	46.8	576.8	21.21	78.2	204.2
Qinghai	114.4	402.5	82.2	0	135.3	2.5	17.5
Xizang	3.4	68	0	0	7.9	1.1	27.3
Sichuan	663	106.2	106.2	0	28.8	21.8	158.6
Ningxia	1596.9	20.5	249.7	0	140.3	4.2	56.9
Hainan	227	7.9	4.3	89.4	5.5	1.5	34

## S4 Supplementary Note (Note S1)

Potentially, we demonstrated the simulation application of the modularized solar evaporator to provide freshwater through gravity-driven separation and photothermal desalination. Here, we

collected the data on power generation structure and industrial-agricultural water consumption over 31 different provinces in China 2021, and used the reverse osmosis technology as a comparison to calculate the CO<sub>2</sub> reduction potential. The following calculation algorithm was constructed to estimate total CO<sub>2</sub> reduction with the modularized solar evaporator:

$$R_{CO_2} = E_{pCO_2} P C_w \eta_{ec} - E_{modularized\ solar\ evaporator}$$

Where  $E_{CO_2}$  and  $p$  were CO<sub>2</sub> emissions per kWh of electricity and weighted power generation over 31 provinces.  $C_w$  and  $\eta_{ec}$  were water consumption over 31 provinces and electricity consumption for water purification through reverse osmosis technology.

### Supplementary References

- [S1] J. Zhao, K. Yu, Y. Hu, S. Li, X. Tan et al., Discharge behavior of Mg–4 wt% Ga–2 wt% Hg alloy as anode for seawater activated battery. *Electrochim. Acta* **56**, 8224-8231 (2021). <https://doi.org/10.1016/j.electacta.2011.06.065>
- [S2] S. Ahuja, *Comprehensive Water Quality and Purification*. (Elsevier Amsterdam, 2014). <https://doi.org/10.1016/b978-0-12-382182-9.00001-3>